# The Thermodynamic Basis of the Saturation Index

## John A. Wojtowicz Chemcon

Thermodynamics (i.e., the laws governing the conversion of heat to and from other forms of energy) is the logical discipline for the mathematical treatment of chemical reactions in homogeneous and heterogeneous systems. The sign of the free energy change as an indicator of the direction of a reaction was known in 1886 (Van't Hoff) under the name "reaction isotherm". The free energy change is a measure of the useful energy available from a system. When applied to solutions of calcium carbonate, the expression for the free energy change for a reaction readily and naturally leads to the calcium carbonate saturation index. The equation that bears Langelier's name, derived from ionic equilibria, is not novel. Therefore, a more appropriate name would be calcium carbonate saturation index as Langelier originally named it (Langelier 1936).

#### Theory

The aqueous solubility equilibrium of calcium carbonate can be expressed by the following reactions:

1. 
$$\operatorname{CaCO}_3$$
  $\smile$   $\operatorname{Ca}^{2+} + \operatorname{CO}_3^{2-}$   $\operatorname{K}_{eq} = {}^{e}\operatorname{K}_{s}$   
2.  $\operatorname{CO}_3^{2-} + \operatorname{H}^+ \smile$   $\operatorname{HCO}_3^ \operatorname{K}_{eq} = 1/{}^{e}\operatorname{K}_2$ 

Overall:

3. 
$$CaCO_3 + H^+ - Ca^{2+} + HCO_3^-$$
  
 $K_{eq} = {}^{c}K_{s} / {}^{c}K_{2} = [Ca^{2+}][HCO_3^-] / [H^+]$ 

Originally appeared in the

Journal of the Swimming Pool and Spa Industry Volume 3, Number 1, pages 35–36

Copyright © 2001 by JSPSI

All rights of reproduction in any form reserved. John A. Wojtowicz – Chapter 2.2 where:  ${}^{\rm e}\!K_{\rm s}$  is the concentration solubility product constant of calcium carbonate and  ${}^{\rm e}\!K_{\rm 2}$  is the second concentration ionization constant of carbonic acid.

The Gibbs free energy change ( $\Delta$ G) for the above reaction is given by (Stumm and Morgan 1996):

4.  $\Delta G = 2.3 RT Log (Q/K)$ 

where:  $\Delta G$  is the free energy (Joules per mol) of dissolution of calcium carbonate, R is the gas constant (8.314 J deg<sup>-1</sup> mol<sup>-1</sup>), T is the absolute temperature in kelvins (i.e., 273 + °C), Q represents the actual composition, and K the equilibrium composition. The ratio Q/K represents the departure of the system from equilibrium. Rearragement leads immediately to the calcium carbonate saturation index (SI):

5.  $\Delta G/(2.3RT) = Log (Q/K) = SI$ 

That this is so can be shown by substitution of the appropriate chemical terms from equation 3, where the subscripts a and e denote actual and equilibrium concentrations, i.e.,  $Q = [Ca^{2+}]_a [HCO_3^{-}]_a / [H^+]_a$  and  $K = [Ca^{2+}]_e [HCO_3^{-}]_e / [H^+]_e$ .

6. SI = Log[Ca<sup>2+</sup>]<sub>a</sub>[HCO<sub>3</sub>]<sub>a</sub>[H<sup>+</sup>]<sub>a</sub>/[Ca<sup>2+</sup>]<sub>a</sub>[HCO<sub>3</sub>]<sub>a</sub>[H<sup>+</sup>]<sub>a</sub>

Since  $[Ca^{2+}]_e[HCO_3^-]_e/[H^+]_e = {}^cK_S^{-/c}K_2$  equation 6 simplifies to:

7. SI = Log  $[Ca^{2+}]_{a}[HCO_{3}]_{a}CK_{2}/([H^{+}]_{a}CK_{3})$ 

Setting  $[HCO_3]_a \cong [Alk]_a$  and expanding the right side of equation 7, gives the calcium carbonate

saturation index with concentrations in mol/L:

10. SI = Log (
$$[H^+]_{e}/[H^+]_{a}$$
) = pH<sub>a</sub> - pH<sub>e</sub> = pH<sub>a</sub> - pH<sub>s</sub>

8. SI = 
$$pH_a + Log [Ca^{2+}]_a + Log [Alk]_a + Log {}^cK_2/{}^cK_s$$

Introduction of factors for converting alkalinity from mol/L to ppm CaCO<sub>3</sub> (–4.7) and calcium from mol/L to ppm CaCO<sub>3</sub> (–5.0), a value of –2.25 for Log  $^{c}K_{2}^{/c}K_{s}$  at 0°C and an ionic strength correction of – 0.34 for 1000 ppm TDS and a correction factor for the temperature dependence of  $K_{2}/K_{s}$  (TC) gives the familiar and updated form of the calcium carbonate saturation index (see part 7 of this series).

9. SI = 
$$pH + Log [Hard] + Log [Alk] + TC - 12.29$$

where [Hard] = calcium hardness and [Alk] = carbonate alkalinity. Another familiar form of the calcium carbonate saturation index is obtained by setting  $[Ca^{2+}]_a = [Ca^{2+}]_e$ ,  $[HCO_3^-]_a = [HCO_3^-]_e$ , and pH = Log 1/[H<sup>+</sup>] in equation 6:

where  $pH_{_{\rm e}}$  is equivalent to  $pH_{_{\rm s}}$  i.e., pH at calcium carbonate saturation.

Equation 10 is the form that Langelier originally expressed the saturation index. He did not transform it to a form such as equation 9 which is often referred to as the Langelier formula or Langelier saturation index. The concept of saturation index for calcium carbonate follows naturally from thermodynamic principles, which were developed in the nineteenth century. Thus, the so-called Langelier Saturation Index, which was derived from ionic equilibria, is not novel. Therefore, a more appropriate name would be calcium carbonate saturation index as Langelier originally called it (Langelier 1936).

The Gibbs free energy change (equation 4) has always been the criterion for judging the spontaneity of chemical reactions via the sign of  $\Delta G$ , as shown by the data in Table 1 (Stumm and Morgan 1996).

$\Delta G = 2.3 RT \log (Q/K)$	Reaction Possibilities
<0 (negative, Q < K)	reaction is possible – $CaCO_3$ can dissolve
$0 (\mathbf{Q} = \mathbf{K})$	system is in equilibrium – ${ m CaCO}_{_3}$ will not dissolve or precipitate
>0 (positive, Q > K)	reaction not possible in forward direction, but possible in reverse direction,
	i.e., CaCO <sub>3</sub> can precipitate

# Table 1 – Reaction Possibilities from Gibbs Free Energy Change CaCO<sub>3</sub> + H<sup>+</sup> — Ca<sup>2+</sup> + HCO<sub>3</sub><sup>-</sup>

### References

- Langlier, W. F. "The Analytical Control of Anti-Corrosion Water Treatment", Journal of the American Water Works Association 28 (1936): 1500–1521.
- Stumm, W. and Morgan, J. J. Aquatic Chemistry, New York, NY: John Wiley & Sons, 3rd edition 1996.
- Van't Hoff (1886) from Glasstone, Samuel. *Thermodynamics for Chemists.* (D. Van Nostrand, New York, NY 1947) p. 283.
- Wojtowicz, J. A. "Swimming Pool Water Balance, Part 7: A Revised and Updated Saturation Index Equation." Journal of the Swimming Pool and Spa Industry 3(1) (1997): 26–32.